

The listing of claims replaces all prior versions and listing of claims in the application:

Listing of Claims:

Claims 1 – 17 (Cancelled)

Claim 18. (Original) A process for converting hydrocarbons comprising contacting a hydrocarbonaceous feed at hydrocarbon converting conditions with a catalyst comprising a zeolite having a mole ratio greater than about 20 of an oxide of a first tetravalent element to an oxide of a second tetravalent element which is different from said first tetravalent element, trivalent element, pentavalent element or mixture thereof and having, after calcination, the X-ray diffraction lines of Table II.

Claim 19. (Original) The process of Claim 18 wherein the zeolite is predominantly in the hydrogen form.

Claim 20. (Original) The process of Claim 18 wherein the zeolite is substantially free of acidity.

Claim 21. (Original) The process of Claim 18 wherein the process is a hydrocracking process comprising contacting the catalyst with a hydrocarbon feedstock under hydrocracking conditions.

Claim 22. (Original) The process of Claim 21 wherein the zeolite is predominantly in the hydrogen form.

- Claim 23. (Original) The process of Claim 18 wherein the process is a dewaxing process comprising contacting the catalyst with a hydrocarbon feedstock under dewaxing conditions.
- Claim 24. (Original) The process of Claim 23 wherein the zeolite is predominantly in the hydrogen form.
- Claim 25. (Original) The process of Claim 18 wherein the process is a process for improving the viscosity index of a dewaxed product of waxy hydrocarbon feeds comprising contacting the catalyst with a waxy hydrocarbon feed under isomerization dewaxing conditions.
- Claim 26. (Original) The process of Claim 25 wherein the zeolite is predominantly in the hydrogen form.
- Claim 27. (Original) The process of Claim 18 wherein the process is a process for producing a C₂₀+ lube oil from a C₂₀+ olefin feed comprising isomerizing said olefin feed under isomerization conditions over the catalyst.
- Claim 28. (Original) The process of Claim 27 wherein the zeolite is predominantly in the hydrogen form.
- Claim 29. (Original) The process of Claim 27 wherein the catalyst further comprises at least one Group VIII metal.
- Claim 30. (Original) The process of Claim 18 wherein the process is a process for catalytically dewaxing a hydrocarbon oil feedstock boiling above about 350 F and containing straight chain and slightly branched chain hydrocarbons comprising contacting said hydrocarbon oil feedstock in

the presence of added hydrogen gas at a hydrogen pressure of about 15-3000 psi under dewaxing conditions with the catalyst.

- Claim 31. (Original) The process of Claim 30 wherein the zeolite is predominantly in the hydrogen form.
- Claim 32. (Original) The process of Claim 30 wherein the catalyst further comprises at least one Group VIII metal.
- Claim 33. (Original) The process of Claim 30 wherein said catalyst comprises a layered catalyst comprising a first layer comprising the zeolite and at least one Group VIII metal, and a second layer comprising an aluminosilicate zeolite which is more shape selective than the zeolite of said first layer.
- Claim 34. (Original) The process of Claim 18 wherein the process is a process for preparing a lubricating oil which comprises:
- hydrocracking in a hydrocracking zone a hydrocarbonaceous feedstock to obtain an effluent comprising a hydrocracked oil; and
- catalytically dewaxing said effluent comprising hydrocracked oil at a temperature of at least about 400 F and at a pressure of from about 15 psig to about 3000 psig in the presence of added hydrogen gas with the catalyst.
- Claim 35. (Original) The process of Claim 34 wherein the zeolite is predominantly in the hydrogen form.

- Claim 36. (Original) The process of Claim 34 wherein the catalyst further comprises at least one Group VIII metal.
- Claim 37. (Original) The process of Claim 18 wherein the process is a process for isomerization dewaxing a raffinate comprising contacting said raffinate in the presence of added hydrogen under isomerization dewaxing conditions with the catalyst.
- Claim 38. (Original) The process of Claim 37 wherein the zeolite is predominantly in the hydrogen form.
- Claim 39. (Original) The process of Claim 37 wherein the catalyst further comprises at least one Group VIII metal.
- Claim 40. (Original) The process of Claim 37 wherein the raffinate is bright stock.
- Claim 41. (Original) The process of Claim 18 wherein the process is a process for increasing the octane of a hydrocarbon feedstock to produce a product having an increased aromatics content comprising contacting a hydrocarbonaceous feedstock which comprises normal and slightly branched hydrocarbons having a boiling range above about 40 C and less than about 200 C under aromatic conversion conditions with the catalyst.
- Claim 42. (Original) The process of Claim 41 wherein the zeolite is substantially free of acid.

- Claim 43. (Original) The process of Claim 41 wherein the zeolite contains a Group VIII metal component.
- Claim 44. (Original) The process of Claim 18 wherein the process is a catalytic cracking process comprising contacting a hydrocarbon feedstock in a reaction zone under catalytic cracking conditions in the absence of added hydrogen with the catalyst.
- Claim 45. (Original) The process of Claim 44 wherein the zeolite is predominantly in the hydrogen form.
- Claim 46. (Original) The process of Claim 44 wherein the catalyst additionally comprises a large pore crystalline cracking component.
- Claim 47. (Original) The process of Claim 18 wherein the process is an isomerization process for isomerizing C₄ to C₇ hydrocarbons, comprising contacting a feed having normal and slightly branched C₄ to C₇ hydrocarbons under isomerizing conditions with the catalyst.
- Claim 48. (Original) The process of Claim 47 wherein the zeolite is predominantly in the hydrogen form.
- Claim 49. (Original) The process of Claim 47 wherein the zeolite has been impregnated with at least one Group VIII metal.
- Claim 50. (Original) The process of Claim 47 wherein the catalyst has been calcined in a steam/air mixture at an elevated temperature after impregnation of the Group VIII metal.

- Claim 51. (Original) The process of Claim 49 wherein the Group VIII metal is platinum.
- Claim 52. (Original) The process of Claim 18 wherein the process is a process for alkylating an aromatic hydrocarbon which comprises contacting under alkylation conditions at least a molar excess of an aromatic hydrocarbon with a C₂ to C₂₀ olefin under at least partial liquid phase conditions and in the presence of the catalyst.
- Claim 53. (Original) The process of Claim 52 wherein the zeolite is predominantly in the hydrogen form.
- Claim 54. (Original) The process of Claim 52 wherein the olefin is a C₂ to C₄ olefin.
- Claim 55. (Original) The process of Claim 54 wherein the aromatic hydrocarbon and olefin are present in a molar ratio of about 4:1 to about 20:1, respectively.
- Claim 56. (Original) The process of Claim 54 wherein the aromatic hydrocarbon is selected from the group consisting of benzene, toluene, ethylbenzene, xylene, naphthalene derivatives, dimethylnaphthalene or mixtures thereof.
- Claim 57. (Original) The process of Claim 18 wherein the process is a process for transalkylating an aromatic hydrocarbon which comprises contacting under transalkylating conditions an aromatic hydrocarbon with a polyalkyl aromatic hydrocarbon under at least partial liquid phase conditions and in the presence of the catalyst.

- Claim 58. (Original) The process of Claim 57 wherein the zeolite is predominantly in the hydrogen form.
- Claim 59. (Original) The process of Claim 57 wherein the aromatic hydrocarbon and the polyalkyl aromatic hydrocarbon are present in a molar ratio of from about 1:1 to about 25:1, respectively.
- Claim 60. (Original) The process of Claim 57 wherein the aromatic hydrocarbon is selected from the group consisting of benzene, toluene, ethylbenzene, xylene, or mixtures thereof.
- Claim 61. (Original) The process of Claim 57 wherein the polyalkyl aromatic hydrocarbon is a dialkylbenzene.
- Claim 62. (Original) The process of Claim 18 wherein the process is a process to convert paraffins to aromatics which comprises contacting paraffins under conditions which cause paraffins to convert to aromatics with a catalyst comprising the zeolite and gallium, zinc, or a compound of gallium or zinc.
- Claim 63. (Original) The process of Claim 18 wherein the process is a process for isomerizing olefins comprising contacting said olefin under conditions which cause isomerization of the olefin with the catalyst.
- Claim 64. (Original) The process of Claim 18 wherein the process is a process for isomerizing an isomerization feed comprising an aromatic C₈ stream of xylene isomers or mixtures of xylene isomers and ethylbenzene, wherein a

more nearly equilibrium ratio of ortho-, meta- and para-xylenes is obtained, said process comprising contacting said feed under isomerization conditions with the catalyst.

Claim 65. (Original) The process of Claim 18 wherein the process is a process for oligomerizing olefins comprising contacting an olefin feed under oligomerization conditions with the catalyst.

Claim 66. (Original) A process for converting lower alcohols and other oxygenated hydrocarbons comprising contacting said lower alcohol or other oxygenated hydrocarbon under conditions to produce liquid products with a catalyst comprising a zeolite having a mole ratio greater than about 20 of an oxide of a first tetravalent element to an oxide of a second tetravalent element which is different from said first tetravalent element, trivalent element, pentavalent element or mixture thereof and having, after calcination, the X-ray diffraction lines of Table II.

Claim 67 – 70 (Cancelled)